



Instrumental Studies of Ni(II) ions onto Zinc Chloride Activated Delonix Regia Shucks Carbon

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- ✓ Instrumental analysis.
- ✓ FTIR, XRD, SEM and EDX

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Abstract

Adsorption of Ni (II) ions as of aqueous solution via activated adsorbent arranged since Delonix Regia shucks Activated with ZnCl₂ (DRZAC) underneath numerous trial set of circumstances. Batch manner adsorption trials were performed. The properties of DRZAC were resolute by SEM, EDX, XRD, FTIR, BET analysis and pH_{ZPC}. The thermodynamic functions like ΔH° , ΔS° and ΔG° were resolute by the van't hoff's plots. Enquiry of these principles presumed that the adsorption was extemporaneous with an increased irregularity and that it was endothermic. XRD and FTIR spectral analysis is systematized as adsorption was physisorption. It has been eminent that the effects of this learning can be used as a greatest adsorbent for the adsorption of Ni (II) ions as of aqueous solution.

1. Introduction:

Heavy metals like Pb, cd, Ni and Cr are hazardous to the environment due to their lack of poisonousness and biodegradability [1]. In heavy metals, nickel is used in the assembly of steel, super amalgams, blends, moneys and cells. Shortest exposure to Ni reasons dermatitis. Some Ni compounds, such as carbonyl are cancer-causing and simply fascinated by the peel [2]. Severe harming of Ni (II) ions causes faintness, biliousness, headache and sickness, chest ache, thirsty cough, wheezing, swift breathing, cyanosis and exciting faintness [3]. Many scientists use various techniques, including chemical reduction or oxidation, biochemical precipitation, ion conversation, film percolation, electrochemical handling, desalination and absorption to remove such heavy metal from contaminated waters. However, greatest of these methods have significant drawbacks, including the removal of incomplete metal, excessive capital, operating costs and disposal of residual metal slabs that are unsuitable for small-scale industries [4].

In many biochemical and corporeal systems, adsorption over activated adsorbent has be situated establish chosen loftier to supplementary modus operandi for the reason that of its ability to effectively absorb dissimilar kinds of adsorbates and the easiness of its project [5]. Nevertheless, commercially existing make active adsorbent are quiet measured costly [6]. As a upshot, numerous scholars have

premeditated low-cost alternatives that are comparatively economical and at one fell swoop have judicious absorption capability. These instructions embrace the usage of fire wood [7], fly dust [8&9], palm fruit cluster [10], stimulated earthen, [11], rice shell [12] coconut bomb [14], hazelnut case [13] and peat [15&16].

The resolution of this learning was towards appraise the probability of using carbon primed since Delonix regia shucks to remove Ni (II) ion as of the aqueous solution. The stimulus of test parameters such as carbon dose, interaction period and preliminary concentrations was investigated. The thermodynamic and instrumental aspects of the adsorption methods were studied.

2. Materials and methods:

2.1 Materials:

The whole thing substances utilized for this experimentation are of AR grade. Adsorbent was primed as of *Delonix Regia* shucks. X- ray Diffraction - DRZAC was analyzed by D8 Focus powder XRD, Bruker corporation and Germany brand. The FTIR spectrascopy was restrained within the range of 400 – 4000cm⁻¹ in a FT- spectrometer, Model- Spectrem one, Make-Perkin Elmer, Version-5.0.1. In IIT madras.

2.2 Preparation of Adsorbent

Delonix Regia shucks were composed from the area in Pondicherry. The Delonix Regia shucks should be washed frequently in condensed water to eliminate mud, grime and contaminants. The wash away shucks were at that time dehydrated in sunshine intended for around 30 days. The dehydrated shucks were cut into minor fries. Biochemical processing of Delonix Regia shucks was activated with ZnCl₂ solution. 20 g of dry Delonix regia shucks were thoroughly varied with 20 ml of ZnCl₂ 1:1 w/v solution to the desired concentration (20%, 40%). The broth was located in an air kiln at 100°C for 24 hrs. This resulted in the carbonation and activation process in a muffle oven for 1 hr at 400°C. The sampler was chilled and then wash away with 0.05 M HCl and then several times with deionized water. It was sieved to the crushed. Particle sizes between 110 mm and 90 mm were in use and retained in the desiccator for supplementary use.

2.3 Physical Categorization of adsorbent

The physical appearance of adsorbent are assumed in Table 1. Total external spaces were planned by means of the BET computation [17].

Table 1: Physico-chemical characteristics of DRZAC

S.No.	Properties	Adsorbent Values
1.	PHzpc	6.0
2.	Constituent part size, mm	90-110
3.	External area (BET), m ² /g	916.1234
4.	Aperture volume, cm ³ /g	0.3986
5.	Aperture size (Pore width), nm	2.7174
6.	Substance density, g/mL	0.52
7.	Stationary Carbon, %	71.11
8.	Humidity content, %	4.36

2.4 Resolution of point of zero charge

Twenty milligrams of adsorbent was added to such a mixture and 50 ml of 50 ppm Ni (II) ions extracted in a 250 milliliters iodine flask was prepared. The preliminary pH standards of the results were attuned

from 2 to 10 via adding 0.1M HCl or 0.1M NaOH. The combinations were permitted toward equilibrate with infrequent shaking for 24 hours. The pH standards of the supernatant liquefied were resolute. The dawn of the preliminary pH and the ending pH of the plot. As of the straight region, pH_{zpc} was evaluated, as revealed in Figure 1 [18].

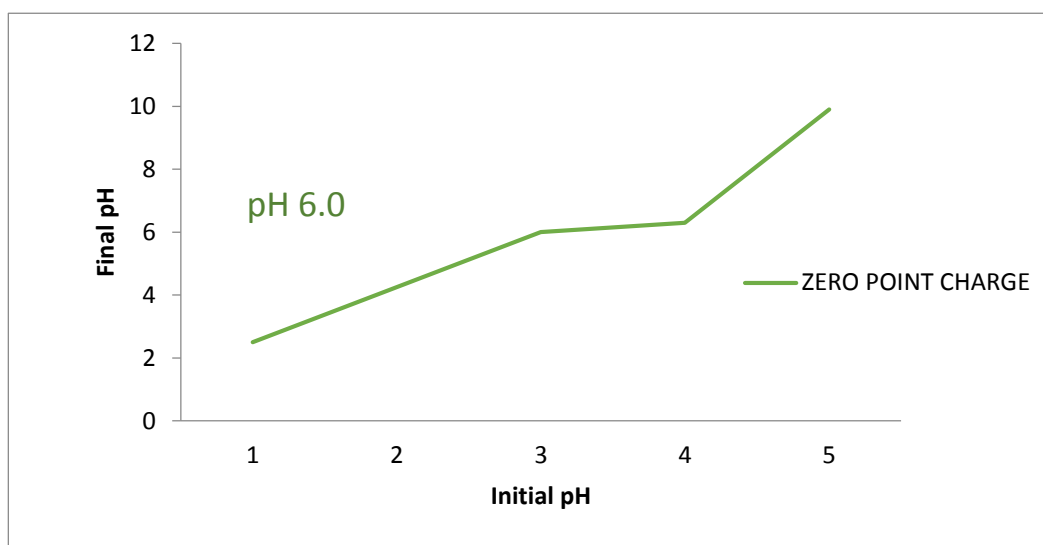


Figure 1: point of zero charge

2.5 Adsorption Experiments

Twenty milligrams of adsorbent was added to 50 ml of known Nickel (II) ions solution in an iodine flask at a predetermined high temperature. The compounds were stirred in a automatic shaker at a rapidity of 180 rpm for predetermined stage intermissions. It was at that time centrifuged. The concentration of the centrifugal metal was resolute by a Systronics double-beam ultraviolet-visible spectrophotometer at 470 nm. The quantity adsorbed at equipoise, q_e (mg/g), was calculated as follows:

$$q_e = C_0 - C_e / W \times V$$

Where, C_0 and C_e (mg/L) are the liquid-phase attentions of Ni (II) ions at the preliminary stage and the symmetry correspondingly. $V(L)$ is the volume of the Ni (II) ions solution and $W(g)$ is the weight of the adsorbent used. The percentage metal exclusion was calculated as:

$$\% \text{ of exclusion} = C_0 - C_e / C_0 \times 100$$

2.6 Effect of temperature

To see the consequence of temperature on the absorption capability, trials are carried out at three dissimilar temperatures (30, 40 and 50°C) using 20mg carbon per 50 ml 10 ppm of the solution. The trial was carried out in a constant temperature water bath. It was perceived that as the temperature was increased, the metal exclusion was also increased [19].

3. Results and discussion

3.1 Effect of Interaction time and preliminary concentration

The effect of interaction time on the proportion removal of metal for dissimilar preliminary concentrations is revealed in Figure 2. The absorption of the metal since the solution upsurges with time and to end with spreads equilibrium at 10, 15 and 80,100 and 120 minutes for the preliminary

concentrations of the adsorbates. 20 mg/L respectively. The percentage of elimination amplified through the upsurge of interaction time and reduced through the upsurge of the preliminary concentration of the metal. Nevertheless, the quantity of metal adsorption in the adsorbent was amplified by growing the preliminary concentration of the metal solution [20], illustrated in Figure 3 and obtainable in Table 2.

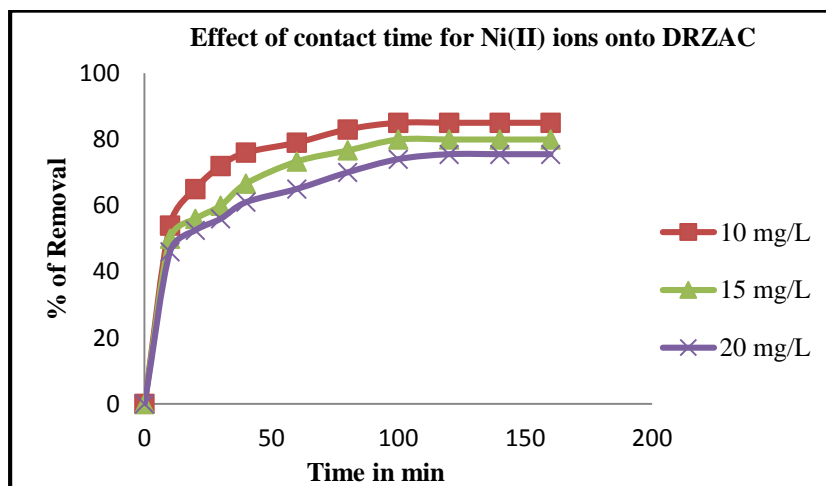


Figure 2: Effect of Contact time and initial concentration

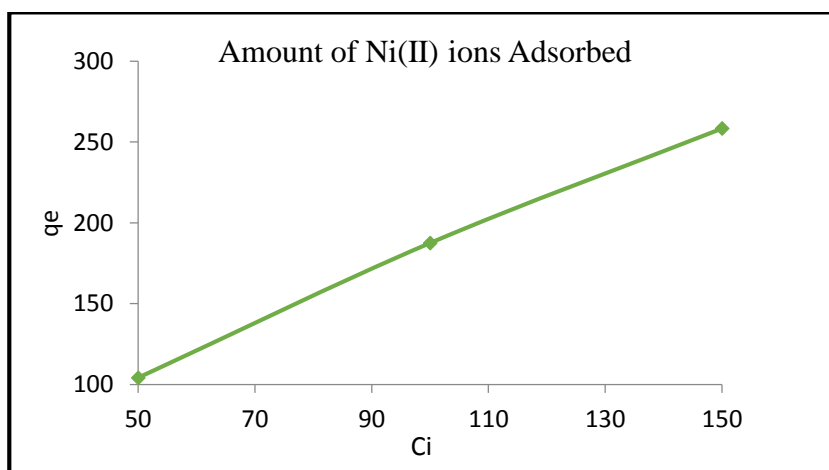


Figure 3: Amount of Ni(II) ions adsorbed at equilibrium

Table 2: Percentage of removal of Ni(II) ions and amount of Ni(II) ions adsorbed

Ci (mg/L)	% of Removal of Ni(II) ions At equilibrium	Adsorption capacity at equilibrium (mg/g)
10	82.50	12.92
15	75.00	16.67
20	70.00	20.00

3.2 Effect of pH

Figure 4 shows the influence of pH on the absorption of Ni (II) ions on the adsorbent. The % upsurge in the exclusion of metal as of the aqueous solution with an upsurge in the pH of the solution. This could be for 2 explanations; one purpose for the accretion of H⁺ ions on the superficial of the adsorbent at low pH may be the extra revolting power towards the metal imminent the adsorbent. As the pH of the solution upsurges up to 7, the accrued concentration on the surface shrinkages, so the dynamic force

on the imminent metal reductions, which helps to upsurge the proportion elimination of the metal solution. Rising the pH since 7 to 14 may upsurge the accretion of OH⁻ ion on surface of the adsorbent, which reasons the small OH⁻ ion to be gradually replaced by the larger metal ion. This influence is additional pronounced as the pH increases from 7 to 14. The second reason is that an upsurge in pH beyond 7 may prompt metal ions. For metal in alkaline media, investigations were accepted out with and without adsorbent at basic pH. The concentration of metal ion solution was originate to be steady in basic-free basic solutions, but metal ion concentrations were establish to lessening in chalky solutions having adsorbents. Thus it is not conceivable to remove the metal ion because of precipitation. Though, other adsorption tests were supported out lone at unbiased pH.

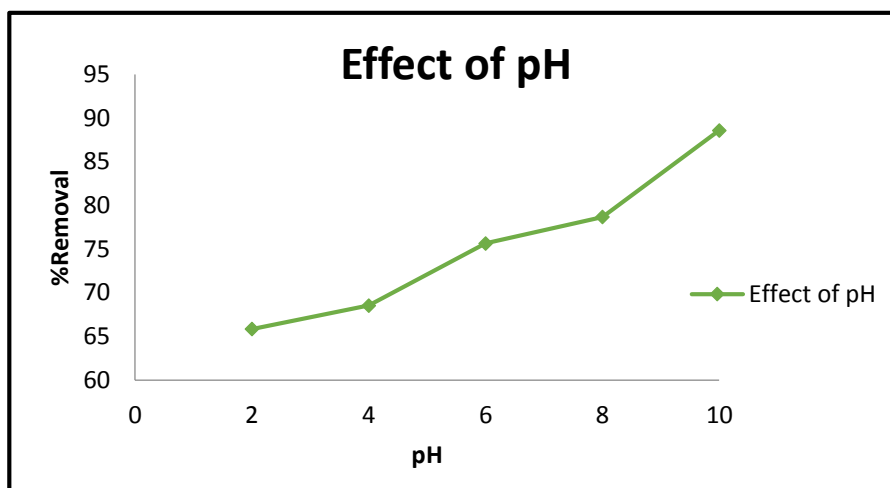


Figure 4: Effect of pH

4. Thermodynamic studies

Thermodynamic limitations like ΔH° , ΔS° and ΔG° were stately based on van't Hoff's plot.

$$\Delta G = -RT \ln K_L \quad (\text{Gibbs Equation})$$

$$\ln K_L = -\Delta H/RT + \Delta S/R \quad (\text{Van't Hoff equation})$$

Where, K_L is the steadiness constant, ΔH° and ΔS° are the standard enthalpy and entropy changes of adsorption respectively and The standards of ΔH° and ΔS° are intended since the slopes and intercepts of the line plot of $\ln K_L$ vs $1/T$. The free energy of explicit adsorption ΔG° (kJ/mol) is intended as of the subsequent appearance

$$\Delta G^\circ = \Delta H^\circ - T\Delta S^\circ$$

The thermo dynamical limits designed since van't hoff plot are assumed in [Figure 5 & Table 3](#). Negative standard free energy of adsorption designates that the adsorption method is satisfactory and extemporaneous in nature. The endothermic nature of adsorption is confirmed by the positive ΔH° values. The bonding amongst Ni(II) ions and DRZAC superficial is very weak, since ΔH° values are found to be in amongst 35.35 to 23.59 kJ/mol. Positive values of ΔS° recommended respectable attraction of the metal to the adsorbent and the adsorption is extemporaneous in nature [21].

5. Instrumental Analysis

5.1 XRD investigation

X ray Deflection images of adsorbent and Ni (II) ions laden DRZAC were revealed in [Figure 6](#). It is apparent from the image that there is no significant alteration in the bands. This may be caused by the fact that adsorption did not adjust the organic environment of the superficial of the adsorbent. These outcomes prime to conclude that the adsorption is physical in environment.

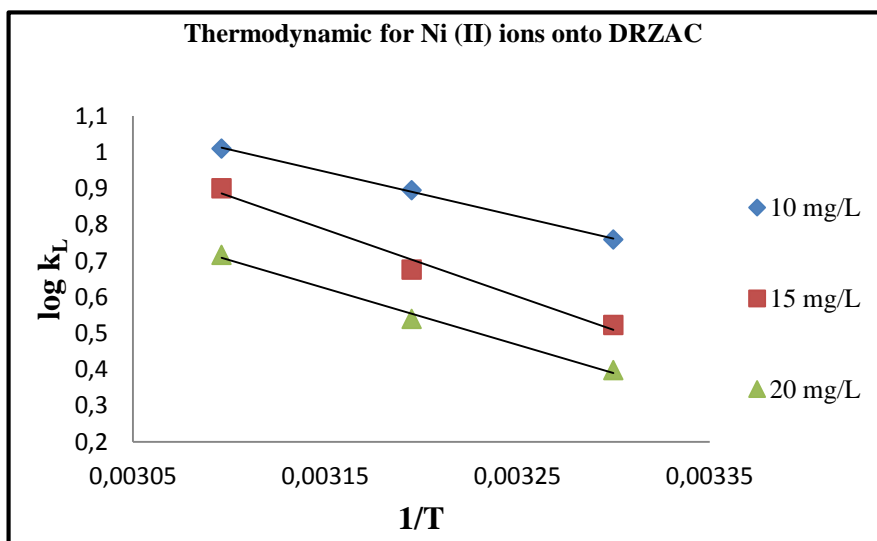


Figure 5: Thermodynamics for Ni(II) ions onto DRZAC

Table 3: Thermodynamics parameters for the adsorption of Ni (II) ions onto DRZAC

Ci mg/L	- ΔG^0 kJ/mol			ΔH^0 kJ/mol	ΔS^0 kJ/mol
	303K	313K	323K		
10	-12.52	-14.10	-15.68	35.35	0.158
15	-8.33	-9.59	-10.88	29.85	0.126
20	-8.22	-9.28	-10.33	23.59	0.105

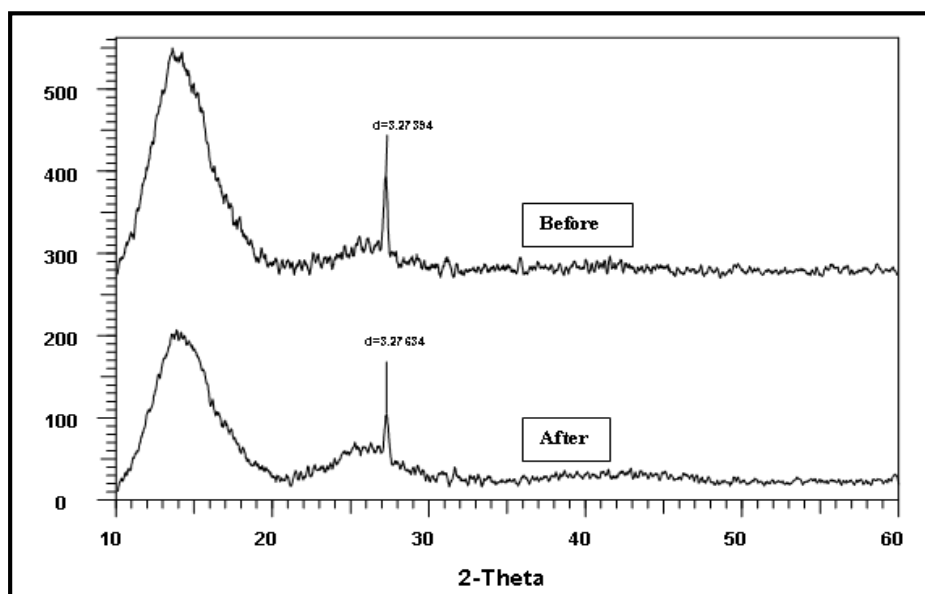


Figure 6: XRD Pattern of DRZAC and Ni (II) ions loaded DRZAC

5.2 FTIR Study

The FTIR range of DRZAC and Nickel (II) ions laden DRZAC was exposed in Figure 7. Alps locations of the beyond band were assumed in Table 4. The gang at 1570.99 cm^{-1} was because to the C = C stretch ambiances and was lifted to 1564.24 cm^{-1} for Ni (II) ions laden asorbent. The band at 1118.11 cm^{-1} and 2358.10 cm^{-1} was due to the C - N stretch and O - H group points were somewhat lifted to 1128.33 cm^{-1} and 2337.92 correspondingly for Ni (II) ions laden adsorbent. These consequences showed the involvement of C = C, C - N and O - H functional group in adsorption process.

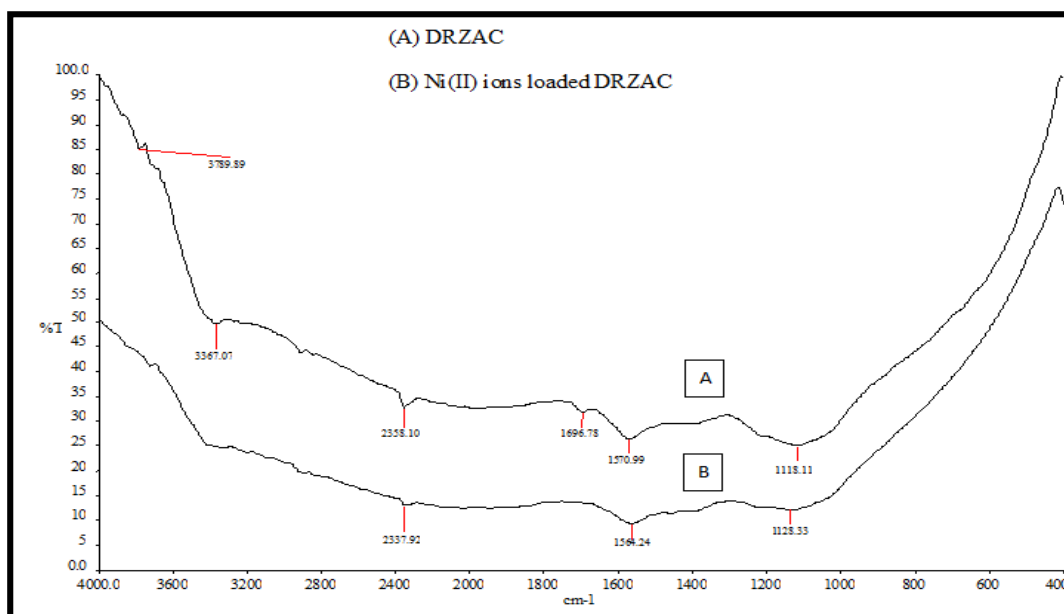


Figure 7: FTIR Spectrum of DRZAC and Ni (II) ions loaded DRZAC

Table 4: Band position of DRZAC and Ni (II) ions loaded DRZAC

S.No.	Band position cm^{-1}		Observation
	DRZAC	Ni(II) ions loaded DRZAC	
1.	3789.89 May be due water adsorption	-----	The peak was disappeared
2.	3368.07 (3400-3250) N-H stretching for 1°, 2° amines	-----	The peak was disappeared
3.	2358.10 (3300-2350) O-H stretch in carboxylic acid group	2337.92	The peak was slightly shifted
4.	1696.78 (1670-1820) C = O stretch in carbonyl group	-----	The peak was disappeared
5.	1570.99 (1400-1600) C=C stretch in aromatic group	1564.24	The peak was slightly shifted
6.	1118.11 (1250-1020) C-N stretch in aliphatic amines groups	1128.03	The peak was slightly shifted

The physical appearance adsorption points observed in the DRZAC at 3789.89 cm^{-1} , 3367.07 cm^{-1} and 1696.78 cm^{-1} was representing H_2O , N – H and C = O stretch were not identified in Ni (II) ions laden

DRZAC. This concludes that H₂O, N – H and C = O functional group of adsorbent was convoluted in mandatory the Ni (II) ions. It is observed that there is no modification in the FTIR design of DRZAC and Ni (II) ions laden DRZAC adsorption amongst the series 400-4000 cm⁻¹. Thus this FTIR spectral learning provisions physisorption.

5.3 SEM Investigation

The superficial morphology of the adsorbent was inspected consuming scanning electron microscopy (SEM), the conforming SEM Micrographs being attained by at hastening voltage of 15 kv at 2500 x and 3.0 kv at 1500 x amplifications (Figure 8). At such amplification, the adsorbent constituent part indicated irregular regions of superficial on which micro holes and macro holes were obviously recognizable.

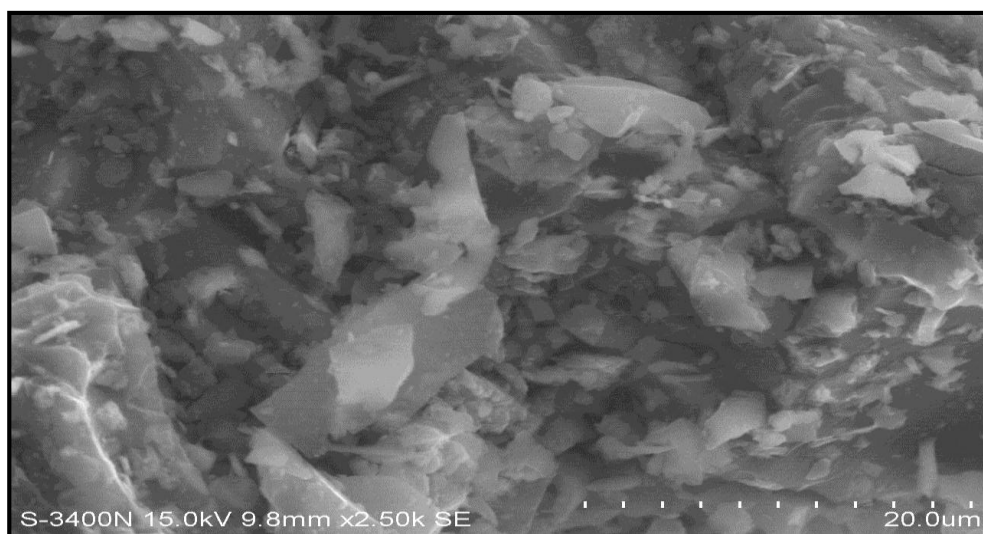


Figure 8: SEM micrograph of DRZAC

5.4 EDX studies for Ni (II) ion loaded DRZAC

EDX investigation of Ni (II) ion laden DRZAC was revealed in Figure 9. The sharp peak of adsorbent laden with Ni (II) indications that Ni (II) ions were bound onto the DRZAC shallow. Points of definite Ni (II) ion are precise slight which concludes the shallow adsorption by Vander Walls force.

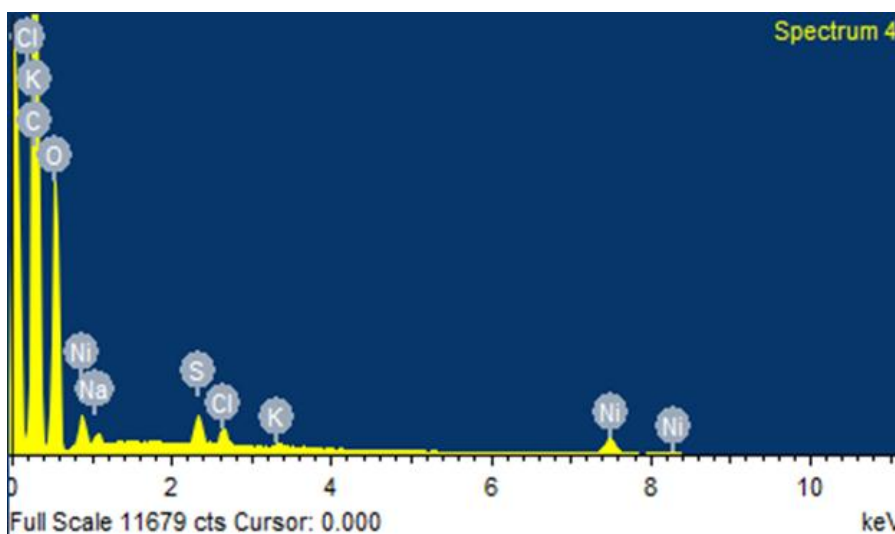


Figure 9: EDX analysis for Ni (II) ion loaded DRZAC

Conclusion

This learning confirmations that adsorbent can be applied efficaciously intended for the exclusion of Ni (II) ions since aqueous solution. The adsorption of Ni (II) ions onto adsorbent amplified through the cumulative of preliminary attentiveness of adsorbates. Thermodynamic limitations such as ΔH° , ΔS° , ΔG° standards concluded that the adsorption was extemporaneous, physical nature and endothermic. The instrumental investigation XRD, FTIR revisions provides clue that adsorption was physisorption with limited chemisorption. SEM representations designated the permeability of adsorbent.

References

1. A.A. Ahmad, B.H. Hameed, N. Aziz, Adsorption of direct dye on palm ash. Kinetic and equilibrium modeling. *Journal of Hazardous Materials*. 141(1) (2007) 70-76. <https://doi.org/10.1016/j.jhazmat.2006.06.094>
2. P.A. Brown, S.A. Gill, S.T. Allen, Metal removal from wastewater using peats. *Water Research*, 34(16) (2000) 3907-3916. [https://doi.org/10.1016/s0043-1354\(00\)00152-4](https://doi.org/10.1016/s0043-1354(00)00152-4).
3. S. P. Brunauer, H. Emmett, E. Teller, Adsorption of gases in multimolecular layers. *J. Am. Chem. So.* 60, (1938), 309-319.
4. De. Chakraborty, S. DasGupta, J.K. Basu, Adsorption study for the removal of a basic dye: Experimental and modeling. *Chemosphere*, 58(8) (2005) 1079-1086. [DOI: 10.1016/j.chemosphere.2004.09.066](https://doi.org/10.1016/j.chemosphere.2004.09.066).
5. V. K. Gupta, A.I. Suhas, V. K. Saini, Removal of rhodamine B fast green and methylene blue from waste water using red mud, an aluminum industry waste. *Ind. Eng. Chem. Res.* 43 (2004) 1740-1747. <https://doi.org/10.1021/ie034218g>.
6. V.K. Gupta, I. Ali, Removal of lead and chromium from wastewater using bagasse fly ash-sugar industry waste. *Journal of Colloid and Interface Science*, 271(2) (2004) 321-328. [DOI:10.1016/j.jcis.2003.11.007](https://doi.org/10.1016/j.jcis.2003.11.007)
7. Ho, Y.S., McKay, G., 2000. The kinetics of sorption of divalent metal ions onto spagnum moss flat. *Water Research*, 34(3) (2000) 735-742. www.elsevier.com/locate/watres
8. C. Karthika, N. Venilamani, S. Pattabhi, M. Sekar,. Utilization of Sago waste as an adsorbent for the removal of heavy metals from aqueous solution Kinetics, Isotherm studies, *Int. J. Engg. Sci. Tech.*, 2(6) (2010) 1867-1879.
9. M. Kobya, Removal of Cr (VI) from aqueous solutions by adsorption onto hazelnut shell activated carbon: Kinetic and equilibrium studies. *Bioresource Technology*, 91(3) (2004) 317-321.
10. K.S. Low, C.K. Lee, Quaternized rice husk as sorbent for reactive dyes. *Bioresource Technology*, 61(2) (1997) 121-125.
11. E. Malkoc, Y. Nuhoglu, Investigation of Nickel (II) from aqueous solutions using tea factory waste, *Journal of Hazardous Materials*, B127 (2005) 120-128, [DOI:10.1016/j.jhazmat.2005.06.030](https://doi.org/10.1016/j.jhazmat.2005.06.030)
12. M. Mohammad, S. Maitra, N. Ahmad, A. Bustam, T. K. Sen, and B. K. Dutta, Metal ion removal from aqueous solutions physic seed hull, *Journal of Hazardous Materials*, 170 (2010) 263-272. [DOI: 10.1016/j.jhazmat.2010.03.014](https://doi.org/10.1016/j.jhazmat.2010.03.014)
13. S.V. Mohan, N.C. Rao, Adsorptive removal of direct azo dye from aqueous phase onto coal based sorbents: A kinetic and mechanistic study. *Journal of Hazardous Materials*, 90(2) (2002) 189-204. [https://doi.org/10.1016/S0304-3894\(01\)00348-X](https://doi.org/10.1016/S0304-3894(01)00348-X)

14. M.M. Nassar, The kinetics of basic dye removal using palm fruit bunch. *Adsorption Science and Technology*, 15(8) (1997) 609-617. <https://doi.org/10.1177/026361749701500806>
15. H. Nollet, M. Roels, P. Lutgen, P.V. Meeren,. Removal of PCBs from wastewater using fly ash. *Chemosphere*, 53(6) (2003) (2003) 655-665. [DOI:10.1016/S0045-6535\(03\)00517-4](https://doi.org/10.1016/S0045-6535(03)00517-4).
16. K. Ramesh, A. Rajappa, V. Roopa, V. Nandhakumar, Kinetics of adsorption of vinyl sulphone red dye from aqueous solution onto commercial activated carbon. *Int. J. Curr. Res. Chem. Phar. Sci.* 1(1) (2014) 28-36.
17. P. Ricou, I. Lecuyer, P.L. Cloirec, Experimental design methodology applied to adsorption of metallic ions onto fly ash. *Water Research*, 35(4) (2003) 965-976. [DOI:10.1016/S0043-1354\(00\)00341-9](https://doi.org/10.1016/S0043-1354(00)00341-9)
18. M. Sachin, R.W. Kanawade, Removal of methylene blue from Effluent by using Activated Carbon and Water Hyacinth as Adsorbent. *Inter. Jour. Chem. Eng. App.* 2(5) (2011) 317- 319. [DOI:10.7763/IJCEA.2011.V2.126](https://doi.org/10.7763/IJCEA.2011.V2.126)
19. M.G. Vieira, A. F. Almeida, Removal of nickel on Bofe bentonite calcined clay in porous bed, *Journal of Hazardous Materials*, 176 (2010) 109-118. [DOI:10.1016/j.jhazmat.2009.10.128](https://doi.org/10.1016/j.jhazmat.2009.10.128)
20. J.R. Weber, W.J. Morris,. Kinetics of adsorption on carbon from solution, *J. Sanit. Eng. Div. ASCE*. 89(SA2) (1983) 31–59.
21. F.C. Wu, R.L. Tseng, R.S. Juang, Kinetics of color removal by adsorption from water using activated clay. *Environmental Technology*, 22(6) (2001) 721-729. [DOI:10.1080/09593332208618235](https://doi.org/10.1080/09593332208618235)

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